

Code :R7322302

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**III B.Tech II Semester(R07) Regular & Supplementary Examinations, April/May 2011**  
**BIOCHEMICAL REACTION ENGINEERING-II**  
**(Biotechnology)**

Time: 3 hours

Max Marks: 80

**Answer any FIVE questions**  
**All questions carry equal marks**

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- What is a bioreactor and what are the duties it is expected to perform?
  - Explain the concept of energy balance and mass balance and how they can be used in biological reaction modelling.
- Give the classification of bioreactors and their configuration. Mention the various applications of bioreactors.
- What are the salient features involved in the design of bioreactors? Enlist them.
  - Derive the steady state design equation of a batch reactor.
- What is a chemostat? Derive the steady state design equation of a chemostat.
  - Obtain the equation of the Monod chemostat model.
- Obtain the design equation of a plug flow reactor.
  - A specific enzyme acts as a catalyst in the fermentation of reactant A. At a given enzyme concentration in the aqueous feed stream (25 lit/min). Find the volume of plug flow reactor needed for 95% conversion of reactant A  $C_{ao} = 2$  mol/liter. The kinetics of the fermentation at this enzyme concentration is given by  

$$A \xrightarrow{\text{enzyme}} R, -r_A = \frac{0.1C_A}{1+0.5C_A} \text{ mol/(liter)(min)}$$
- What are the reasons for non ideal behaviour of reactors? Explain the concept of macrofluid and microfluid.
  - A particular fermentation is to be carried out in a chemostat. Before carrying out the actual fermentation, it was decided to evaluate the flow characteristics of the chemostat by introducing a tracer in the form of a pulse input. The time versus concentration of the tracer data are given in the table below.

Time, min	0	10	20	30	40	50	60	70
Concn. of trace, g/l	0	2	6	7	5	3	1	0

Find the average residence time and plot the E curve. Also find the variance.
- Discuss in detail about immobilized packed reactors and their applications in bioprocessing.
- Explain the basic concepts of scale up of bioreactors.
  - Write about non dimensional analysis.

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- Define bioreactor. What are the requirements it is expected to cope up with?
  - Discuss the concepts of energy and mass balances in biological reaction modelling.
- How are bioreactors classified? Give the characteristics features of various bioreactors and their applications.
- What are the various ideal flow reactors? Explain them briefly.
  - Discuss about batch bioreactor design briefly.
- Obtain the design equation of a single stage chemostat starting from material balance.
  - Derive the equation of the Monod chemostat model.
- Derive the general design equation of a plug flow reactor.
  - A gaseous feed of pure A (2 mol/liter, 100 mol/min) decomposes to give a variety of products in a plug flow reactor. The kinetics of the conversion is represented by  $A \rightarrow 2.5(\text{products})$   $-r_A = (10 \text{ min}^{-1})C_A$ . Find the expected conversion in a 22 liter reactor.
- State the reasons for non ideality of reactors. What is the difference between a microfluid and a macrofluid?
  - A particular fermentation is to be carried out in a chemostat. Before carrying out the actual fermentation, it was decided to evaluate the flow characteristics of the chemostat by introducing a tracer in the form of a pulse input. The time versus concentration of the tracer data are given in the table below.

Time, min	0	10	20	30	40	50	60	70
Concentration of tracer, g/l	0	2	6	7	5	3	1	0

If the vessel is to be used for fermentation of molasses which obeys an overall first order reaction kinetics with  $r = 0.3 \text{ h}^{-1}$ , find the fractional conversion of the reactant.
- Discuss in detail about fluidized bed reactors and their applications in bioprocessing.
- Write about the design and analysis of air lift bioreactors and their application in animal cell culture.

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- Define bioreactor and what are the requirements it is expected to cope up with during fermentation process.
  - Explain the concept in mass and energy balance, and in biological reaction modeling.
- Describe the characteristic features of different types of bioreactor and mention their application. In submerged and solid state fermentation.
- Explain the design of total bioreactor.
  - What are the various methods of fed- batch/ semi- batch fermentation processes? Explain with their method of feeding.
- Derive the expression for concentration of reactant in the exit stream for N equal size CSTRS connected in series. Assume first order reaction.
  - Define dilution rate and cell productivity. Explain the dependence of effluent substrate concentration cell concentration and cell production rate on dilution rate as per Monod chemostat model.
- What are the characteristic features of plug flow? Derive the performance equation of a plug flow reactor.
  - A stream of pure gaseous reactant A ( $C_{Ao} = 660$  m mol/liter) enters a plug flow reactor at a flow rate of  $F_{Ao} = 540$  m mol/min and polymerizes there as follows:  $3A \rightarrow R$ ,  $-r_A = 54$  m mol/liter .min. How large a reactor is needed to lower the concentration of A in the exit stream to  $C_{Af} = 330$  m mol/liter/.
- What are the reasons for deviation from ideality in flow reactors? Explain microfluid and macrofluid.
  - The concentration readings given in the table below represent a continuous response to a pulse input into a closed vessel which is to be used as a chemical reactor. Calculate the mean residence time of fluid in the vessel and plot the E curve. Also find the variance.

Time, min	0	5	10	15	20	25	30	35
Concen.gm/liter	0	3	5	5	4	2	1	0
- Discuss briefly about:
  - Packed bed reactors and
  - Fluidized bed reactors, with emphasis on their use in bioprocessing.
- Write about the design and analysis of fed batch reactors and their application in animal cell culture.

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- Give the definition of a bioreactor and also mention the duties it is required to perform.
  - Discuss briefly about the concepts of mass and energy balance, and biological reaction modelling.
- Write about the classification of bioreactors and their configurations. Mention the various applications of bioreactors.
- Explain the concepts of reactors based on flow characteristics.
  - Explain the design of ideal batch reactor using material and energy balance and derive the performance equation.
- Define chemostat and derive the equations of the Monod chemostat model.
  - Explain the concepts of dilution rate and productivity.
- Explain plug flow behavior and derive the design equation of a plug flow reactor.
  - An aqueous feed containing A(1 mol/liter) enters a 2 liter plug flow reactor and reacts away ( $2A \rightarrow R$ ,  $-r_A = 0.05C_A^2$  mol/liter.sec ). Find the outlet concentration of A for a feed rate of 0.5 liter/min.
- List the reasons for which non ideality prevails in the flow pattern of reactors? Explain the concept of macrofluid and microfluid.
  - The concentration readings given in the table below represent a continuous response to a pulse input into a closed vessel which is to be used as a chemical reactor

Time, min	0	5	10	15	20	25	30	35
Concen.mg/liter	0	3	5	5	4	2	1	0

If this vessel is to be used as a reactor for a liquid decomposing with rate  $-r_A = k C_A$ ,  $k = 0.307 \text{ min}^{-1}$  find the fraction of reactant unconverted in the real reactor.
- Discuss about the application of tubular reactor concept in immobilized packed bed reactors and fluidized bed reactors, and their use in bioprocessing industry.
- Describe the process of scale up of bioreactors briefly.
  - Write a brief note on non- dimensional analysis.

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